

CO-DIGESTION AND MODELLING ANAEROBIC PROCESSES THROUGH THE BIOWIN SOFTWARE

Co-Digestion and Modelling Anaerobic Processes through the Biowin Software

Student's Name

Professor

Course

Date

Table of Contents

Co-Digestion and Modelling Anaerobic Processes through the Biowin Software	1
ABSTRACT	3
Co-Digestion and Modelling Anaerobic Processes through the Biowin Software	4
1.1 Background	4
1.2 Problem statement	5
1.4 Significance	6
LITERATURE REVIEW	6
2.1 Biogas Generation	6
2.2 Important Considerations	8
2.3 Biochemical Methane Potential (BMP)	12
2.4 BioWin software	14
METHODOLOGY	15
3.2 Model calibration methods	15
3.3 Biomethane potential experimental protocol	16
RESULTS AND DISCUSSION	18
4.1 Waste Characterization	18
4.2 Bio Methane Potential	19
4.3 BioWin simulation	20
CONCLUSION	20
References	22

ABSTRACT

This study encompasses the integration pilot-scale experiments, bio-methane potential (BMP) evaluation and BioWin which will give insight the biogas potential by combining several substrates including sheep manure scraps. BioWin 3.1 model helped in predicting possible results and analyze synergies of different proportion ratios for sheep manure, food waste. BMP was utilized to determine and characterize the kinetics of biogas production in batch mode.at the laboratory, batch bioreactors of glass jars 250 ml each was used room temperature. The batch reactor at a temperature of around 36° C at different proportions of the mixture composition and the actual results were compared to BioWin predicted results. Through the experimental process daily, BMP (biochemical methane production) was recorded as the digestion process was going on. The anaerobic co-digestion combinations exhibited higher biogas production levels as compared to per single substrate digested. BioWin software models proved to be a vital predicting as previous research indicated as the model successfully predicted COD reduction rates, biogas production yields.

Co-Digestion and Modelling Anaerobic Processes through the Biowin Software

With the world population numbers increasing by the millions, the demand for food supplies has increased rapidly. At every particular point food production, processing, retailing, distribution organic waste and food by-products are encountered and this brings out a big quest in management of waste. Burdened to achieve a viable energy production, the existing untapped potential in agriculture and organic waste crops up, existing technologies and innovations can be utilized to bring about a solution into the realization of organic waste as a reliable source of renewable energy such as biogas (Fraga et al., 2019).

1.1 Background

Around the globe, anaerobic digestion of waste is a critical entity to ensuring sanitation, health with an aesthetic setting a favorable environment capturing cleanliness, by the use of medium and large wastewater treatment at a domestic and industrial level. Across history, developments and improvements of the concept of aerobic digestion involving various types of organic wastes have been perfected. With the high level of waste output, sludge generated across different specialties such as local agricultural farms as tanneries, dairies, pig farms and abattoirs to advanced manufacturing industries such as meat processing, sugar cane industries, water treatment plants. Food waste is common around the globe due to increases population levels, business and household activities this bringing about the need to have an efficient process of managing waste. Farms around the world in rural settings produce manure which is an important source of fertilizer and with anaerobic digestion, one can generate renewable gases (Harms, H., Schlosser, D., & Wick, L. Y. 2011).

Around cities in the world, anaerobic ponds and treatment plants are easily customizable to an operator's specific needs in construction. Anaerobic digestion provides various aspects in waste management, such as it reduces pathogens, eliminates unpleasant stench, and inhibits putrefaction rates. Chiefly it provides an essential source of biogas. Biogas is a mix of gas of methane around 66%, around 30% is CO₂, and other gases with further purification biogas earn natural gas sets. The challenge exists that of measuring biogas production at various locations as an experimental phase of a project, thus various computer software has been

developed to come up with models that can simulate predict and simulate anaerobic digestion results and indicators, an example of this software include BioWin, GPS-x, WEST, SIMBA, Aquifas , SimuWorks, WRc, and STOAT. Each of the simulator software has specific strengths and weaknesses depending on their application and the required task ahead. The diverse features and unique capabilities of these software categories vary in speed, customization features, interactive environment, presentation of results, operation preferences; a powerful tool for different applications (Rasi et al. 2011).

BioWin software by EnviroSim has proved to be more flexible and effective in simulating wastewater treatment systems. Notable features such as the friendly user-compatibility make it a more leading modelling tool compared to platforms such as WEST and GPS-X. These software platforms are capable of predicting the parameters and bring about a correlation with experimental data (Dursun et al., 2011).

1.2 Problem statement

With the advancement of industries and processing plants around the world, high levels of organic waste are generated daily around the world. The problem of organic waste is a pertinent one, ranging from meat industries to agricultural farms to the food industry a lot of organic waste is generated daily such as food waste, manure, solid waste. These waste products if not recycled they bring about unpredictable and unprecedented gas emissions of potent greenhouse gases such as methane. This calls for better alternatives to deal with food waste, solid waste to provide beneficial end products such as biogas and also fertilizers.

From all these a big potential exists of a generation of biogas, the mixing of food waste into wastewater treatment plants in cities and also in farm digesters as proved to produce more biogas. Innovating successful prediction of the anaerobic digestion process output capacity may require one to do experimentation. This is time-consuming and expensive. Computer software simulation provides a clear guide for anticipated outcomes providing a more cost-effective model (Dursun et al., 2011). The hypothetical models in computer simulation can predict various outcomes such as overload to the system ensuring thus one can have a clean anaerobic treatment system in real life.

1.4 Significance

This thesis offers information that will be critical for startups by elucidating critical data on co-digestion and anaerobic digestion systems to maximizing the efficiency of the existing models. Also, it will provide significant economic benefits for facilities facing low methane gas production, limited treatment facilities, Biogas generation systems are a revenue opportunity for various farms, industries, benefiting from waste into essential sources of energy such as electricity makes one self-dependent.

1.5 Objectives

The study targets to create a prediction model for co-digestion utilizing BioWin software at the same time comparing real-time results from a pilot-scale batch reactors experiment comparing checking the biogas production levels among different combinations of substrates. This study aims to develop a working model simulating anaerobic and co-digestion process for animal manure and food waste. This model will help in developing strategies for increasing gas production and optimizing anaerobic digestion.

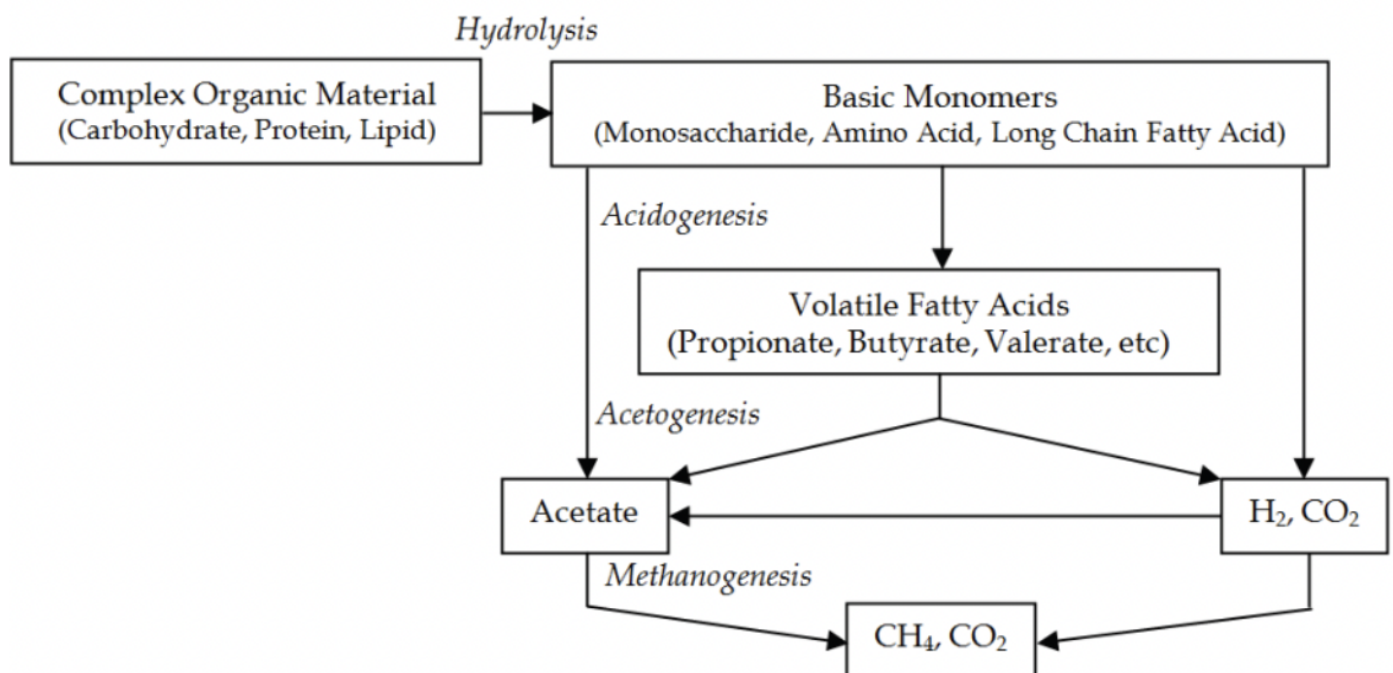
LITERATURE REVIEW

2.1 Biogas Generation

The treatment of various forms of waste makes use of anaerobic digestion (AD) as the standard procedure used to treat high – strength organic wastes ranging from the treatment of wastewaters solids to animal manure, to industrial waste from industries such as tanneries, piggeries, dairies, meat production industries. The Anaerobic digestion is the decomposition and analysis of organic matter process in an environment deprived of oxygen by bacteria and microbial communities' possetting fermentative and methanogenic qualities. These transform organic matter to solid residual, biogas (methane) and other gases such as carbon dioxide. Food scraps, biosolids, fats and oils (FOG) can all be digested to produce methane similar to natural gas (McCarty, 2012).

The organic waste treatment makes use of the advantaged of anaerobic digestion of waster in ensuring stabilization of sewerage sludge from around various cities, municipalities around the globe. Batstone et al., 2002 clarifies that the anaerobic digestion is often divided into a three-step process with enzymatic hydrolysis, fermentation (acidogenesis), and the final step methanogenesis. The initial step, hydrolysis encompasses the transformation of biological material by bacteria, to carbohydrates lipids, proteins. Fermentation of the products and other substances generated from the first by acidogenic microorganisms produces organic acids and hydrogen. Fermenting bacteria further oxidize the organic acids to produce hydrogen and acetic acid. The intermediates are transformed by methanogenic microorganisms transforms the hydrogen and acetic acid into methane (McCarty, 2012).

Biogas production in anaerobic digesters is increasingly gaining interests among various stakeholders in most countries. Anaerobic digestion is an important process due to the benefits that are acquired from environmental and economic aspects as it reduces the volume of the materials thus it helps in alleviating soil pollution and also producing affordable gas as a renewable affordable source of energy.



The expenditures of constructing anaerobic digesters are significantly higher as compared to uncovered digesters. However, the anaerobic digesters have anaerobic ponds bring about significant advantages odor regulation, spiking of the decomposition process increased biogas yields at the same time reducing greenhouse gases released. In dairy farms, manure management helps to improve on the aesthetic environment of farms, reduces chances of contamination. Solid residuals from the digestion process provide organic manures which reduce the dependency to chemical manures and fertilizers.

In some setups digestion of food waste in anaerobic treatment facilities will results to the buildup of fats, oils and grease thus spiking the risk of clogging of pipe systems and pumps present in the public sump systems as well as wastewater handling amenities. Separating food waste from the sewerage system set-up to a separate set up anaerobic digester saves on resources and prevents sewer overflows.

2.2 Important Considerations

The waste disintegration process incorporates sensitive pathways with particular key parameters and optimum environmental requirements. For optimum levels of biogas production and waste breakdown, these factors have to be considered. Environmental and operational factors affect the hydrolytic and fermentative working of the microorganisms present in the digester systems.

Environmental factors	Operational parameter
<ul style="list-style-type: none">• Temperature• pH• Alkalinity• total volatile solids (VS),• waste characteristics• COD• BOD• Carbon-nitrogen proportions(C/N)• organic loading rate (OLR)• total solids (TS),• volatile fatty acids (VFA)	<ul style="list-style-type: none">• (SRT) solid retention• (HRT) hydraulic retention• digester design• digester mixing

TVS Total volatile solids

This is determined by the type of materials that are used in the digestion process it describes the number of solids that are broken down into other forms. The biodegradable solids present in waste has an impact on parameters such as C/N, loading rate (OLR). Maximum AD operations occur in a situation where the materials have high volatile solids and low-non biodegradable material (RVS) as the biodegradable fractions affect bio-degradability. Materials with high levels lignin have little VS levels thus they cannot be used as favorable sources for methane biogas production.

Carbon –Nitrogen fraction

The C/N constituents levels of a substance is an important parameter that affects the overall biogas yield. This ratio affects the methanogens activity thus affecting gas production; an elevated C/N ratio reduces the effectivity of anaerobic digestion implying that methanogens are rapidly consuming of nitrogen leading to decreased biogas yields. . On the other hand, with too much nitrogen is present a very low C/N ratio exist this is toxic to methanogens activity due to the accumulation of ammonia and unfavorable pH. For optimum performance, a suitable C/N ratio 20-30% has to be adopted to be able to maintain stability and favor bacterial and microbial activity.

Nutrients

As critical nutrients for methanogenesis bacteria metal ions have been found to improve the performance of anaerobic systems these include cobalt, nickel, molybdenum provides the ideal condition for methane production while other metals are important in stimulating methanogenic action metals, including selenium, molybdenum, boron, manganese, and aluminum.

Biochemical Oxygen Demand

BOD is the overall portion for the effectiveness of an AD, it is the level of biodegradable constituents in a substance present in sludge is used as a metric for the overall effectiveness of an AD.

Chemical oxygen demand

The COD reflects the level of microbial activity in relation to degradation. The

COD provides the amount of oxygen present in a sample that is used up in a reaction. The BOD and COD of a substance checking the biodegradability level in the digestion system.

OLR

This is the quantification of the capacity anaerobic digester for biological conversion. It is quantified levels of biological matter flowing into a digester over a particular time. It is an important parameter for avoiding overloading of the digesters and the reduction of inhibiting factors such as accumulation of fatty acids.

pH

The pH of a digester creates the optimum environment for microorganisms to operate in maintaining the optimal anaerobic digestion. Appels, et al. (2008) in the previous study advises that the optimal pH range is between 6.5-7.6. The anaerobic process destabilization of the pH can be caused by the amassing of intermediate acids which bring about pH drop in the fermenting phase. To achieve a running stable environment, bicarbonate or carbonate entities are supplemented to neutralize the acidity caused by the existing carbonic acid and from VFA also stabilizing alkalinity in the buffer to (Chen, 2010).

Temperature

Temperature influences other parameters and various processes such hydrolysis rate and methane formation these include Mesophilic temperature ranges 30 and 38° C, thermophilic 55° C. Selecting of operating temperature in a digester is critical to ensuring an efficient process and the maintenance of a stable environment. The methanogenesis bacteria and microbial communities activity is temperature based and are very sensitive to temperature changes. Thermophilic digestion operates at higher levels than mesophilic digestion thus may have higher levels of loading rates and also pathogen destruction.

Alkalinity

Carbonic acid from carbon dioxide is the main contributor to acidity in the digester system and not volatile fatty acids, an optimum alkalinity level is 2000 to

5000 mg/L. Sodium bicarbonate, lime, or sodium carbonate bring about auxiliary alkalinity mixing.

Co digestion

A combination of more than two substrate and feedstocks in Anaerobic digestion to create a suitable and optimum environmental condition for maximum gas production among other factors diverting from the traditional mono digestion anaerobic approach where a single substrate is used. The mono digestion approach has been encountered by weaknesses such as imbalanced nutrients; inhibiting factors materials this has made anaerobic co-digestion approach targeting several feedstock sources at once to become a widely held exploration area with an effort to improve conservative AD expertise. Co-digestion comes through as a process to help overcome limitations of using a single substrate thus affects the normal levels can result into increased treatability, improved pH, provide alkalinity .food scraps, plant material, fats, oils and grease have become important substrates.

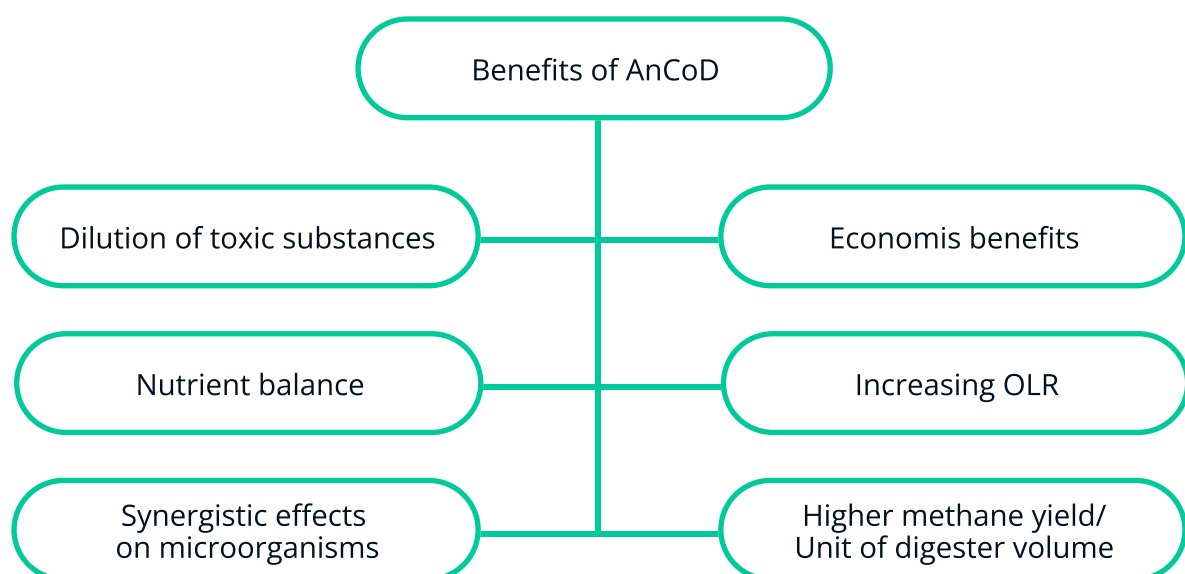
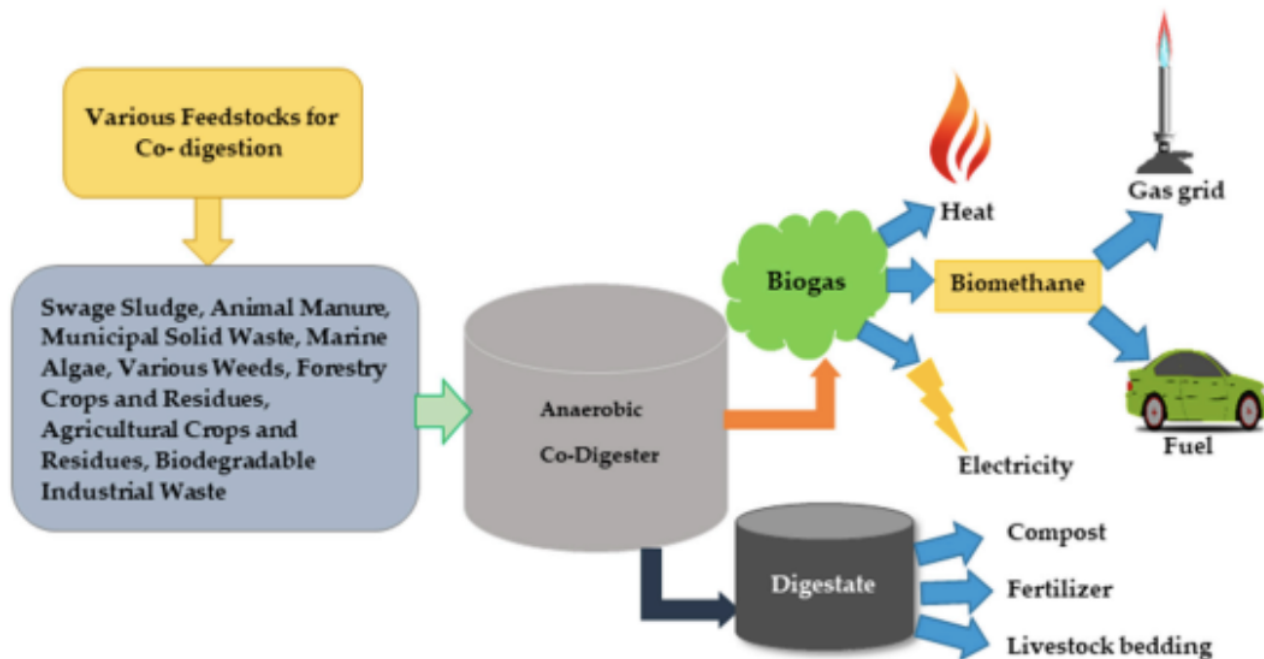


Figure 2 co-digestion advantages

Research has proved that the use of co-substrates has had an upscale in the levels of biogas levels in digesters. Synergy combination of different co-substrates and the supply of absent nutrients by food waste and FOG organic materials when added into the main substrate such as dairy (Murto M. et al 2004).



In the last few years, anaerobic co-digestion (AnCoD) has gained acceptance due to its enhancement of conservative AD technology and also due to its economic sustainability, improved methane yields, the capability to ease the existing shortcomings from mono-digestion which bring about infectivity.

2.3 Biochemical Methane Potential (BMP)

These experiments are efficient in predicting the methane potential and biodegradability factors of various substrates (Rabii et al., 2019). This modus operandi involves the substrate of interest being mixed with an anaerobic bacteria culture acquired from existing working digesters and kept at a steady temperature (mesophilic or thermophilic). The bottled mixture is constantly mixed over a period of 30 to 60 days. In the process of incubation, the substrate undergoes anaerobic breakdown discharging methane and carbon dioxide gases (Achinas S et al 2019). An inoculum supply in BMP is made up the microorganism which set the precedence in

the anaerobic breakdown progression bringing about the activation of process. It comprises one of the most critical of the BMP factors with important consideration being brought to its origin, time of sampling, composition, concentration as it has the ability of significantly influencing results and efficiency of the BMP. Mixing impacts the dissemination of microorganism, supplements, substrate, and alkalinity among other parameters within the digester substance and avoiding of sediment formation of materials and evening out temperature conveyance within the digester.

In BMP different techniques and strategies are utilized in the quantification of the rate and volume of biogas production. Not limited these include the use of transducers, volume displacement devices lubricated syringes, pressure manometers or. Gas chromatography is used in identifying and quantification of the collected gases.

Reactions within the batch reactor system bring about degradation of the organic contents found in the substrate occurs through a series of complex microbiological processes resulting to biogas release and production in the incubation phase until no biodegradable substances are left. With biogas production being the most important factor in the calculation of the methane potential of various constituents and the biodegradability of a substrate. It is important that the BMP process collects the biogas without any leaks and losses and chances of resulting to error. The need to have counter errors and bring about a correction to the factors to capture the observed methane potential based on the conditions of temperature and pressure. This brings about the issues of quality control in the BMP.

The BMP test results are important simulations that can predict the overall performance of a real-time biodegradability of substrates conditions (Elbeshbishy et al, 2012).

Therefore the formula for the calculation of BMP could be as follows:

$$BMP = \sum_{n=1} \frac{X_n}{S}$$

Where BMP is the biochemical methane potential, X is the daily production of methane, n is the unit of time and S is the amount of initial substrate of the sample added. Methane yields from the experiment are quantified to determine methane

potential of a particular substrate and this is reflected as chemical oxygen demand (COD) or even in terms of biodegradability. BMP is a technique useful in laboratory scale to quantify the conversion of biological waste to CH₄. The experimental value of BMP is given as CH₄/g VS ml added to the reactor (Sanchez et al, 2016), but can also be expressed in m³CH₄/m³ sample, ml CH₄ / Kg sample or ml CH₄ / kg COD added (Owen et al, 1979).

BMP similar to computer models and mathematical model provides predictions to be used in the designing of a full-scale digester system. The central setback set by BMP setups is the lack of standardization processes many researchers have been proposed with different volumes, test inoculum, the substrate to microorganism ratios, methane and nutrients measuring devices Luna-del Risco et al 2011.

2.4 BioWin software

The BioWin software is used all around the globe as a waste treatment simulation software models capturing various aspects to come up with simulations are important guides for engineers and operators to that there is increased effectivity in treatments at an affordable budget. The main users are construction engineers and owners, manufacturing industries, academic institutions that use it to design, upgrade and optimize treatment plants. In bio win software one can generate various aspects of waste treatment such the indicators such as oxygen demand both BOD and COD. Elbeshbishy et al. established a strong association between simulated predictions by the BioWin with experimental results while utilizing the software. Key Parameters and fractions in digesters systems can be predicted accurately thus BioWin proves to have the unlimited capability in simulating large systems of wastewater treatment notwithstanding other diverse elements such as anaerobic digesters. Dhar et al 2011) BioWin software is capable in predicting the decomposition of organic compounds parameters as the same order as experienced and experimental level results.

The BioWin software possesses twofold functioning components; a constant steady setting and a second one dynamic emulator. When predicting and simulating systems with constant conditions a steady-state module is more appropriate while the dynamic simulator can predict the more dynamic behavior of wastewater systems with varied operating conditions. The dynamic BioWin ASDM model

comprises of about fifty state variables parameters and sixty process expressions describing biological processes, chemical reactions in AD systems.

A BioWin prototypical model that predicts and demonstrate possible outcomes and benefits in biogas production levels from co-digestion and anaerobic digestion of incorporating food waste into sheep manure. To operate and do a startup of an anaerobic digester requires one to possess robust knowledge and skills partly which can be gained from past experiences, experiments. These processes are time-consuming and may not be cost-effective. Computer simulations offer an efficient cost-effective alternative for predicting, optimization of operations eventually leading to an efficient digestion and this improves on biogas release levels (Dursun et al., 2011).

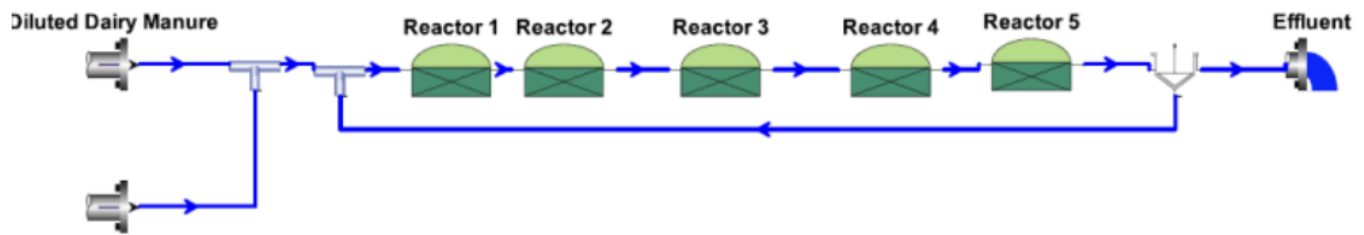
METHODOLOGY

This section describes the various steps that were undertaken in this research in fulfilling the objectives of the study.

3.1 Biogas modelling

BioWin uses a large number of expressions, default factors and kinetic rate for describing an ideal biological process which can be customized to fit various circumstances. It has the successfully simulate large and complex wastewater handling plants because it includes most of the elements in wastewater treatment plants with the ability to simulate more complicated processes by simply combining elements (multiple processes) together. BioWin one can predict risks factors such as overloading digesters, methane quantification, requirements and solid waste depletion rates specific to food waste breakdown. Important parameters that can be evaluated are methane gas production rates, volatile solid destruction rates, volatile solids and chemical demand loading rates, thermophilic and mesophilic operating temperatures.

This study assimilates a BioWin model, designed and calibrated to the assist in predicting the impact and possible benefits of incorporating food wastes into sheep manure for biogas production as compared to purely the use of sheep manure only. For the study objectives, A BioWin model 3.1 was set up to simulate the performance of a multi-stage mesophilic digester anaerobic digester as shown below.



Average values of COD, Total Kjeldahl nitrogen (TKN), alkalinity, total phosphorous (TP), pH of were the chosen parameters for this study. In the model, the digester HRT was set up to be 30 days which is the value of the pilot experiments.

3.2 Model calibration methods

BioWin provides the user with a hypothetical digester system allows one to come up with the optimum conditions. In this study, one aims at analyzing the possible outcomes of the co-digestion combinations of food waste and sheep manure in different proportions.

Calibration of the BioWin model to fitting AD conditions requires on to know hydrolysis rate which is essential to initial stage of the reaction series thus in BioWin it affects the efficiency of the digester, an increase in the hydrolysis rate will results to increased efficiency of the digester also reducing of COD levels in effluents. The value of COD is dependent of the fractions as described below F_{us} , (F_{bs}) (F_{us}) and (F_{up}) , adjusting these fractions has a direct effect on the COD.

Parameter	Fraction of
Fbs	total influent COD
Fac	readily biodegradable COD
Fxsp	biodegradable influent COD)
Fup	total influent COD
Fp04	influent total phosphorus

3.3 Biomethane potential experimental protocol

3.3.1 Batch experiment set up

For an efficient bioreactor set up, various factors have to be considered. Sheep manure, food waste were chosen as the substrates in this experimental process. The food waste consists mainly of boiled rice, the egg remains. The specific aims of this experiment are to determine the biogas yield of co digested mixtures as compared to mono-digestion setups.

The inoculum in this set up was acquired from an existing digester. It was stored and maintained at a temperature of 6°C to conserve an active microbial activity. Three days before the use it was reactivated at 37°C. Sheep manure (MS), Food waste was acquired from existing farms these were stored in a cool dry environment. As guided by Esposito et al 2012 batch-test are important models in predicting the effect of possible combination of mixtures on the AD results. The experimental set up adopted laboratory glass of 250 ml capacity were utilized, the working volume of 200ml as the anaerobic digesters.

Mixtures ratio came up resulted in six setups, two for mono-digestion (sheep manure, food waste), inoculum, MS: FW 70:30, MS: FW 50:50 and MS: FS 30:70 and inoculum (blank reactor). In the above ratios, the glass bottles were filled microbial inoculum, pure water and substrates in the estimated quantities and washed with Nitrogen for a period 5 minutes and sealed. After this they are placed in a rotary incubator at 36°C and pH was maintained at pH 8 for a period of 30 days (706 hours). Three bottles per mixture were set up to ensure accuracy and reduction of chances of error. This study measured identified parameters COD and the methane generation rate over a period of 30 days.

Number of bioreactors	Substrates content
1	Inoculum 100%
2	Sheep manure(MS) 100%
3	Food waste(FW) 100%
4	MS: FW 70:30
5	MS: FW 50:50
6	MS: FW 30:70

Generally, BMP tests require three test groups a blank, control and substrate. These groups of combinations are tested in the experiment in groups of three per set up to achieve high levels of reproducibility and increasing the reliability of the procedure used to acquire the results from the tests and to enhance clear arithmetical analysis. In this study substrates bottles MS, FW were filled the inoculum and their respective the substrate and co-substrate and nutrients added. The blank which acts as the control is filled with the inoculum, distilled water in the place of the substrate to assimilate the background of methane release from the organic materials and enzymes bacteria existing in the inoculum. The control in this study is important as it helps in determining the precision and accuracy of the BMP tests.

Analytical methods

Key parameters in this study as TS total solids (VS) volatiles were estimated as guided by standard procedures. The pH was quantified by the use of a pH meter. Micro gas chromatography was used to evaluate the methane gas levels release. Alkalinity was measured using a titration method. Helium gas was used as a carrier gas.

RESULTS AND DISCUSSION

4.1 Waste Characterization

Characterization phase provides an important phase in this study the substrates; sheep manure, food waste are summarized in the table below. The table below shows the physicochemical parameters of the substrates.

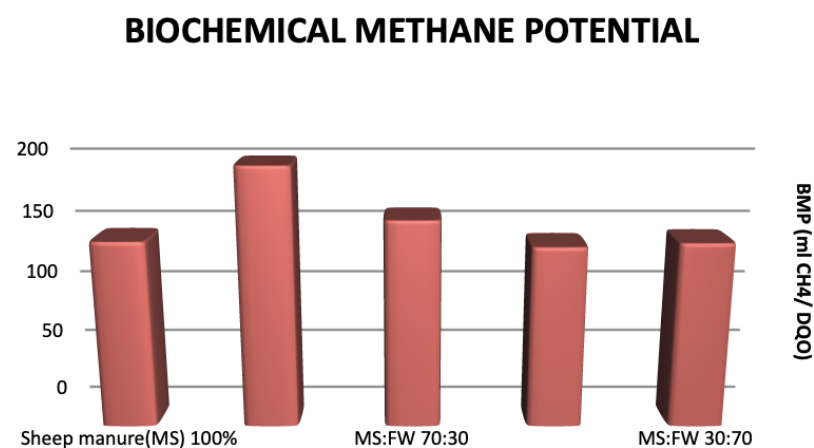
Substrate	COD(g/L)	pH	TS (g/L)	TVS (g/L)	TS/TVS
Inoculum	24.11	7.1	37.6	18.37	0.5
Food waste	128.9	4.1	157.54	146.64	1.08
Sheep manure	300	9.46	368.76	296.97	1.24

From the above result, it is clear that there are diverse characteristics in the values of COD, TS,TVS are highest in the sheep manure, the sheep manure is more acidic from the pH and the food waste are more alkaline. The second level of characterization is

Bromatological parameters of waste these include substrates composition ratios that are lipids, fibres, TKN, protein, carbohydrate, humidity, and ashes.

Substrate	Lipids %	Fibre %	TKN	protein	carbohydrates	humidity	ashes
Inoculum	Not present	Not present	4.98	28.8	Not present	98.4	Not present
Food	9.5	10.4	2.62	17.5	73.3	83.5	7
Sheep manure	13.9	17.5	2.88	17.76	45.7	30	24.5

4.2 Bio Methane Potential



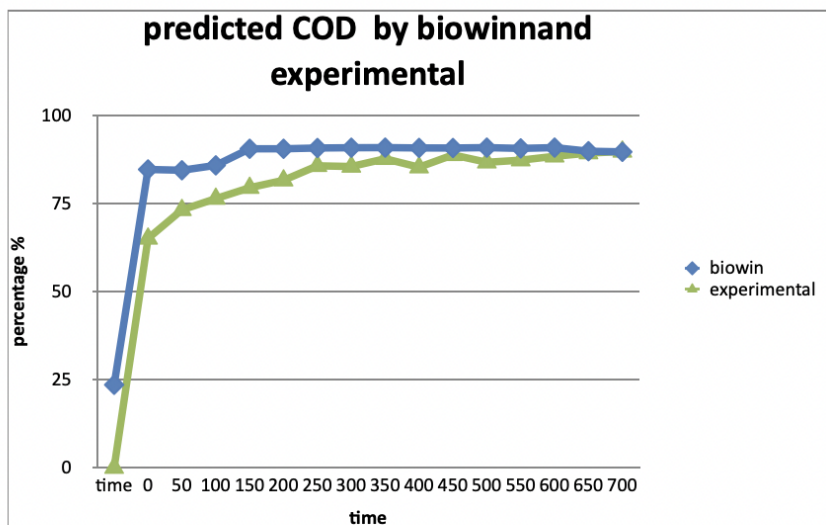
From the above graph the results of all treatments BMP levels performance with the highest levels being 212 ml/CH₄/Gcod, from this experimental study it is clear that co digestion upshots into increased levels of BMP as compared to mono-digestion.

Biogas production

In terms of mono-digestion set ups the highest biogas production was found in treating 100% FW. Food waste provides a good substrate to add to various combination as it has high digestively, however using high levels of FW can bring about high levels of VFAs, ammonia which bring about bioreactor instability.

4.3 BioWin simulation

The characteristics in the batch reactors were modeled into the BioWin software model to predict biogas release. The graph below represents the batch results from COD elimination of sheep manure from the batch reactor and also BioWin simulation. The graph represents the results gained from the actual COD results from the experimental assay, and the predicted quantity by BioWin recorded in the all-inclusive time during the experimentation.



CONCLUSION

Anaerobic batch reactors also offer important simulation that can be used to predict various parameters in anaerobic digestion and co-digestion. Pretreatment technologies can be utilized to increase the biogas production Levels and also reduce limitations using food waste an example is microwave treatment of the food has high chances of increasing biogas production. In terms of performance co-digestion, there were higher levels in biogas release than individual mixtures.

Computer simulations are a critical technology to water treatment as they can achieve dynamic formations efficiently; from this evaluation, the BioWin model predicted with accuracy various parameters such as COD, methane accumulation among others. The BioWin provides a clear picture that can help one to understand the expected capacity of a particular set up. The hypothetical digesters potential risks can also be revealed, and help in planning.

A comparison of mono-digestion systems and the optimization by the

co-digestion performance it can be observed that one has to do a keen selection of microbial communities and substrates. These have an important contribution to the enhancement of the inclusive overall outcome of the digestion process and biogas harvested quantities thus co-digestion is an important contributor to reducing operating costs. This eventually results in achieving quality products with a decrease in the levels of environmental pollution levels and carbon release footprint at the same time supporting both the local farms and eventually impact national economies.

The mixing together of substrates to achieve co-digestion have shown to have greater feasibility above mono-digestion models. Adopting this approach enhances the performance thus extra biogas release is accomplished. Use of unconventional co-substrates made a difference upgrade anaerobic absorption of nourishment. These co-substrates, by and large, brought about in expanded every day methane generation, higher methane division in biogas.

Also, BioWin model prediction is an important entity, from the set model in this study predicted with a high likelihood of agreement of key factors such as biogas production, COD and VS reduction, and ammonia and VFAs levels. From the above investigation, it is clear of the importance of simulations on prediction important factors to ensure improved biogas levels. Customization of the BioWin set values is a useful strategy in ensuring the accuracy and precision of models and also when dealing with undetermined parameters.

References

- Achinas S, Euverink GJW. Elevated biogas production from the anaerobic co-digestion of farmhouse waste: Insight into the process performance and kinetics. *Waste Manag Res.* 2019;37(12):1240-1249. doi:10.1177/0734242X19873383
- Appels, L., Baeyens, J., Degreve, J., & Dewil, R. (2008). Principles and potential of the anaerobic digestion of waste-activated sludge. *Progress in energy and combustion science*, 34(6), 755-781.
- Batstone, D.J., Keller, J. (2003). Industrial applications of the IWA anaerobic digestion model No. 1 (ADM1). *Water Science and Technology*, 47 (12), 199-206
- Boltes, K., Leton, P. & Garcia-Calvo, E. (2008). Volatile fatty acid anaerobic degradation: Kinetic modeling with an inoculum under controlled conditions. *Industrial and Engineering Chemistry Research*, 47(15), 5337-5345
- Dhar, B. R., Elbeshbishy, E., Hafez, H., Nakhla, G., & Ray, M. B. (2011). Thermo-oxidative pretreatment of municipal waste activated sludge for volatile sulfur compounds removal and enhanced anaerobic digestion. *Chemical engineering journal*, 174(1), 166-174.
- Dursun, D., Jimenez, J., & Bratby, J. (2011). Moving Forward in Process Modeling: Integrating Anaerobic Digester Into Liquid Stream Models. *Proceedings of the Water Environment Federation*, 2011(17), 728-741.
- Elbeshbishy, E., Nakevski, A., Hafez, H., Ray, M., & Nakhla, G. (2010). Simulation of the impact of SRT on anaerobic digestability of ultrasonicated hog manure. *Energies*, 3(5), 974-988.
- El-Mashad, H. M., & Zhang, R. (2010). Biogas production from co-digestion of dairy manure and food waste. *Bioresource technology*, 101(11), 4021-4028.
- Esposito G, Frunzo L, Gioerdano A, et al. (2012. a) Anaerobic co-digestion of organic

wastes. *Reviews in Environmental Science and Bio/Technology* 11: 325–341

Esposito G, Frunzo L, Liotta F, et al. (2012. b) Bio-methane potential tests to measure the biogas production from the digestion and co-digestion of complex organic substrates. *The Open Environmental Engineering Journal* 5: 1–8

Fraga GL, Teixeira CFJ, Ferreira ECM. (2019) The potential of renewable energy in Timor-Leste: An assessment for biomass. *Energies* 12: 1441

Fyfe, J. (2013). Characterisation, monitoring and dynamic modelling of a two-stage stabilisation pond system supporting reuse and recycling of dairy shed effluent.

Ghanimeh S, Abou Khalil C, Ibrahim E. (2018) Anaerobic digestion of food waste with aerobic post-treatment: Effect of fruit and vegetable content. *Waste Management & Research* 36: 965–974

Harms, H., Schlosser, D., & Wick, L. Y. (2011). Untapped potential: exploiting fungi in bioremediation of hazardous chemicals. *Nature Reviews Microbiology*, 9(3), 177-192.

Lansing, S., Botero, R. B., & Martin, J. F. (2008). Waste treatment and biogas quality in small-scale agricultural digesters. *Bioresource technology*, 99(13), 5881-5890

Lauwers, J., Apples, L., Thompson, I.P., Degreve, J., Impe, J.F.V., Dewil, R. (2013). Mathematical modeling of anaerobic digestion of biomass and waste: power and limitations. *Progress in Energy and Combustion Science*, 39, 383-402.
doi: 10.1016/j.pecs.2013.03.003

Luna-del Risco M, Normak A, Orupõld K. (2011) Biochemical methane potential of different organic wastes and energy crops from Estonia. *Agronomy Research* 9: 331–342.

Murto, M., Björnsson, L., & Mattiasson, B. (2004). Impact of food industrial waste on anaerobic co-digestion of sewage sludge and pig manure. *Journal of environmental*

management, 70(2), 101-107.

Rabii A, Aldin S, Dahman Y, et al. (2019) A review on anaerobic co-digestion with a focus on the microbial populations and the effect of multi-stage digester configuration. *Energies* 12: 1106